



## OPERATIONAL CONDITIONS AFFECTING LOW-TEMPERATURE DRYING ASSISTED BY POWER ULTRASOUND

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## Introduction

## WHY EXPLORING THE USE OF LOW-TEMPERATURE DRYING in Solids and Pastes

HOT AIR DRYING:

**PROS:** 

- + Low cost
- + Simple unit operation

### CONS:

- High energy consuming
- Quality loss in biomaterials (high stress)
  - Structural damage
  - Nutritional damage (vitamins, etc...)



From http://www.arakawa-mfg.co.jp/

FREEZE DRYING OR LYOPHILIZATION



# Introduction

## WHY EXPLORING THE USE OF LOW-TEMPERATURE DRYING in Liquids

## SPRAY DRYING (ATOMIZATION):

**PROS:** 

- + Good quality
- + High productivity (Simple operation)

## CONS:

- Nozzles

- High viscosity liquids



From <u>www.bete.co.uk</u>

FREEZE DRYING OR LYOPHILIZATION



# Introduction

## FREEZE-DRYING OR LYOPHILIZATION





# Introduction

## LOW-TEMPERATURE CONVECTIVE DRYING

Use of air temperatures below standard room conditions (T<15-20 °C):

T>T<sub>freezing</sub> (Evaporation) T<T<sub>freezing</sub> (Sublimation, Atmospheric Freeze drying)

### **PROS:**

- -No Vacuum (Continuous processing)
- -Low investment
- -Liquids, solids and pastes
- -Similar quality than freeze-drying
- -Chemical, pharmaceutical,.....

## CONS: VERY SLOW!!!!







## **ALTERNATIVES FOR LOW-TEMPERATURE DRYING INTENSIFICATION:**

Thermal energy:

Direct increase of drying air temperature

Thermal technologies: Microwave

**Infrared radiation** 

High risk of product overheating

Mechanical energy:

Power ultrasound (US)

**Higher cost** 

Not developed technology

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**Recent advances** in the design of efficient air-borne ultrasonic devices have been carried by the Power Ultrasonics Group (CSIC, Spain and PUSONICS) and their feasibility for hot air drying intensification has been tested in collaboration with the ASPA Group (Universitat Politecnica de València, UPV, Spain).



**CYLINDRICAL RADIATOR (CR)** 



**STEPPED PLATE RADIATOR (SPR)** 



Table. Compendium of previous works carried out by UPV and CSIC groups addressing theapplication of power ultrasound on convective drying.

REFERENCE	PROCESS VARIABLE UNDER STUDY	MATERIAL BEING TESTED	ULTRASONIC DEVICE*
Gallego-Juarez et al., 1999	Air temperature and ultrasonic power	Carrot	SPR
Gallego-Juarez et al., 2007	Air temperature and velocity and ultrasonic power	Carrot and apple	SPR
Mulet et al., 2003	Ultrasonic power	Carrot	SPR
Garcia-Perez et al., 2011	Ultrasonic power	Eggplant	CR
Ozuna et al., 2011a	Ultrasonic power	Potato	CR
Garcia-Perez et al., 2012a	Product structure and ultrasonic power	Orange peel	CR
Garcia-Perez et al., 2009	Product structure and ultrasonic power	Lemon peel and carrot	CR
Puig et al., 2012	Product structure and ultrasonic power	Eggplant	CR
Carcel et al., 2010	Mass load density	Carrot	CR
Garcia-Perez et al., 2006b	Air velocity, mass load and ultrasonic power	Carrot	CR
Garcia-Perez et al., 2007	Air velocity	Lemon peel, persimmon and carrot	CR
Carcel et al., 2007	Air velocity	Persimmon	CR
Garcia-Perez et al., 2012b	Air temperature	Eggplant, carrot and apple	CR
Garcia-Perez et al., 2006a	Air temperature	Carrot	CR

\* CYLINDRICAL RADIATOR (CR), STEPPED PLATE RADIATOR (SPR)





"Thereby, this work aims to show the influence of air velocity and temperature, two of the most important operational parameters, on Low-Temperature Drying assisted by power ultrasound."



# **Materials and Methods**

### **RAW MATERIAL:**

- Materials with very different internal structure have been used.
- Structure has been characterized by macroscopic and microscopic analysis :

**Density and porosity measurements** 

- **SEM and Cryo-SEM observations**
- Instrumental texture tests have been performed.



EGGPLANT

APPLE

CARROT







**DRYING TESTS**:

### **PROCESS VARIABLES:**

- Air velocity (from 1 to 6 m/s)
- □ Air temperature (from -14 to 10 °C)

**DIFFUSION MODELS** were used to describe the water transport mechanisms during drying, as well as to quantify the influence of power ultrasound on kinetic parameters.



EFFECTIVE DIFFUSIVITY, D<sub>e</sub>

**EXTERNAL COEFFICIENT, K** 



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## **Results and Discussion**

### Influence of raw material:





Influence of material structure on air-borne ultrasonic application in drying



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			D <sub>e</sub> (10 <sup>-11</sup> m²/s)	VAR (%)
0.1 0.2 0.3 0.4 0.5 0.6 0.7 0.8		AIR	1.1±0.1	99.3
Z (MRayl) Figure, Influence of acoustic impedance on TC and ultrasonic	Carrot	AIR+US	3.1±0.3	91.8
performance for hot air drving operations (Ozuna et al., 2014a).		Increment (%)	<mark>182</mark>	
	Apple	AIR	1.6±0.4	98.0
Drying Technology, 30: 1199–1268, 2012 Copyright (): 2012 Taylor & Francis Group, LLC ISSN: 073-307 crist(1): 2023-200 colline		AIR+US	5.5±1.1	93.3
DOI: 10.10/80/07 17 39 17 201 2.675 53 1		Increment (%)	<mark>244</mark>	
Intensification of Low-Temperature Drying by		AIR	4.8±1.3	93.4
Les V. Carrie Para <sup>1</sup> Less A. Carrel <sup>1</sup> Ensieue Piere <sup>2</sup> Carrier Parallé <sup>3</sup> and	Eggplant	AIR+US	15.8±3.3	92.3
Juse v. Garcia-Ferez, Juan A. Carcel, Enrique Riera, Carmen Rossello, and Antonio Mulet <sup>1</sup>		Increment (%)	<mark>229</mark>	

Table. Influence of ultrasonic application on effective moisture diffusivity

for low-temperature drying (-14 °C) (Garcia-Perez et al., 2012).

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#### Intensification of Low-Temperature Dryin Using Ultrasound



## **Results and Discussion**

### Influence of raw material





Raw Product (Homogeneous frozen product) Beginning of drying (water removal by sublimation)



□ Uniform Retreating Ice Front (URIF) models for freeze drying (T  $\leq$  T<sub>freezing</sub>)

**\Box** FROZEN CORE + EXTERNAL POROUS LAYER  $\rightarrow$  Low acoustic impedance (Z)

**\Box** It is being reduced the influence of internal structure  $\rightarrow$  Similar behavior



## **Results and Discussion**

### Influence of air temperature



Figure. Cryo-SEM image of apple cubes AIR dried at 10 °C.

-10 °C



300µm

Figure. Cryo-SEM image of apple cubes AIR dried at -10 °C.

- **Drying at -10 °C involves a more porous structure.**
- Any remarkable effect of US was observed on product structure.



## **Results and Discussion**

### Influence of air temperature



Figure. Drying kinetics of apple cubes at 10 °C (Santacatalina et al., 2014).

□ Larger effects of US at temperatures below freezing point (-10 °C, more porous structure)

Figure. Drying kinetics of apple cubes at -10 °C (Santacatalina et al., 2014).



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## **Results and Discussion**

### Influence of air temperature



Figure. Drying kinetics of eggplant cubes (8.5 mm) at different air velocities and temperatures.



## **Results and Discussion**

### Influence of air velocity



Figure. Drying kinetics of eggplant cubes (8.5 mm) at different air velocities and temperatures.

- The higher the air velocity, the faster the drying.
- **D** The same effect is observed at the different temperatures.
- The increase of air velocity reduces the external resistance to mass transfer (greater turbulence in the air/product interface)



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## **Results and Discussion**

### Influence of air velocity



Figure. Drying kinetics of eggplant cubes (8.5 mm) at different air velocities and temperatures.

- The typical effect is observed at 10 and -10 °C (the higher the air velocity, the faster the drying).
- At 0°C, the opposite behavior was found (the higher the air velocity, the slower the drying)

#### **WHY**???

- Water removal causes the temperature reduction (close to product freezing)
- Ultrasound could contribute to the product freezing
- A portion of the energy is employed for nucleation and less amount of energy is assigned for mass transport improvement. 19



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## **Results and Discussion**

### Influence of air velocity

			Air velocity (m/s)			
T (ºC)			1	2	4	6
-10	AIR	D <sub>e</sub> (10 <sup>-10</sup> m²/s)	1.44 <sub>a</sub>	1.20 <sub>a</sub>	1.34 <sub>a</sub>	1.48 <sub>a</sub>
		K (10 <sup>-3</sup> kg w/m²/s)	0.44 <sub>a</sub>	0.52 <sub>a</sub>	0.74 <sub>ab</sub>	0.95 <sub>b</sub>
		VAR (%)	99.8	99.5	99.6	99.7
		EMR (%)	4.1	6.4	7.6	4.1
	AIR+US	D <sub>e</sub> (10 <sup>-10</sup> m²/s)	8.40 <sub>b</sub>	11.05 <sub>ь</sub>	10.01 <sub>b</sub>	10.85 <sub>ь</sub>
		K (10 <sup>-₃</sup> kg w/m²/s)	1.46 <sub>c</sub>	2.22 <sub>d</sub>	3.07 <sub>e</sub>	3.55 <sub>f</sub>
		VAR (%)	99.1	99.5	99.9	99.7
		EMR (%)	7.6	4.6	3.8	4.3
		∆D <sub>e</sub> (%)	485	824	645	631
		∆ <b>K (%)</b>	227	322	313	271

Table. Modeling of drying kinetics of eggplant cubes (8.5 mm) at -10 °C and different air velocities.

- **US** improved both internal (D<sub>e</sub>) than the external (K) mass transport.
- The increased was more marked on  $D_e$  (up to 824%) than K (up to 313%).
- The influence of air velocity on US performance was negligible at -10 °C (FLUIDIZED BED DRYING OPERATION)



•The feasibility of power ultrasound to improve low-temperature convective drying of foodstuffs has been confirmed.

•Ultrasound was able to speed-up both internal and external water transport, but the effect was more marked in internal transport.

•Air velocity and temperature are significant variables affecting the lowtemperature drying assisted by power ultrasound.

•Although, the effect was different to that found in hot air drying operations.

•The scaling-up of ultrasound technology for drying operations is still a challenge ahead.





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